

Advanced controls - fuzzy logic for fluidized bed boiler

Tero Joronen, Rupert Kerschbaum

Abstract

Fluidized bed combustion is a good technology for burning wet and varying fuels with low flue gas emissions and high efficiency. A supervisory level control application constantly controls CFB [Circulating Fluidized Bed] or BFB [Bubbling Fluidized Bed] combustion to minimize flue gas emissions (NO_x [nitrogen oxides], SO_2 [sulfur dioxide], and CO [carbon monoxide]), improve combustion efficiency, and reduce use of limestone, ammonia and auxiliary fuels. Combustion symmetry is controlled by means of balancing the fuel feed. Fuzzy logic is used to create controls and optimization functions in this multivariable and non-linear process. Fuzzy logic should be the fine-tuning for every BFB and CFB.

Keywords: Fluidized Bed Combustion, Fuzzy Control, Emission Control, Process Optimization

Introduction

In the Finnish paper and pulp industry the share of fluidized bed technology in burning solid fuel has remarkably increased recently. The first energy solution for FBB was implemented in 1970's and after that the technology has been studied and utilized a lot. Finnish research in the field of combustion technology has been conducted in the form of a program since 1988, when the Energy Department of the Ministry of Trade and Industry launched the first phase of the LIEKKI-program (Hupa and Matinlinna 1998). The research is continuing as the CODE-program [Modeling Tools for COMbustion Process DEVELOPMENT]. One part of the program is to study overall combustion kinetics of solid fuel in a fluidized bed boiler (Hupa 2000). This information is used also to design advanced control systems. For decades the control of fluidized bed boilers has been a great interest of studies (Pyykkö and Uddfolk 1997, Joronen 2000, Keyes and Kaya 1984, Criswell 1980, Nyström 1983, Tuovinen and U. Kortela 1988, Karppanen 2000, Markkula et al 2000, Kortela et al 1994).

Modern fluidized bed combustion technology has proven itself to be a way of efficiently disposing of large quantities of waste water sludge, paper production wastes and other mill wastes while meeting the latest flue gas emission requirements (Kokko and Niemelä 2000, U.S. Department of Energy 2000). Fluidized bed combustion has become a lower cost alternative to older grate technology. The most important feature controlling a fluidized bed boiler is bed control, which means maintaining the proper fluidization and temperature profiles in the furnace. This demand corrects air and fuel controls. Traditionally combustion optimization has been left to an operator. Making corrections to running models is usually difficult; it is necessary to make adjustments constantly. The operators do not usually have the time or sometimes the skills to do this. Solutions to manage the combustion have been sought from process automation. While automation manages the combustion, load changes and variation in fuel quality get paid special attention and conditions in the furnace are optimized irrespective of load level or prevailing fuel (Joronen 2000).

Metso Automation has developed an advanced combustion control application, which runs as an integrated part of metsoDNA (Metso Automation's Dynamic Network of Applications). The application utilizes measurements existing in the standard instrumentation level, including on-line O_2 and CO measurements, together with measurements from the most significant online emission analyzers. The application provides set point and parameter outputs to the basic controls. The application consists of two levels - the coordination level, which stabilizes the process, and the supervisory level, which optimizes the process. The supervisory level control methods are based, among other things, on fuzzy logic. This advanced combustion control application is made up of several subsystems, and contains displays for basic operation, tuning and follow-up (Pyykkö and Uddfolk 1997, Joronen 2000, Markkula et al 2000)].

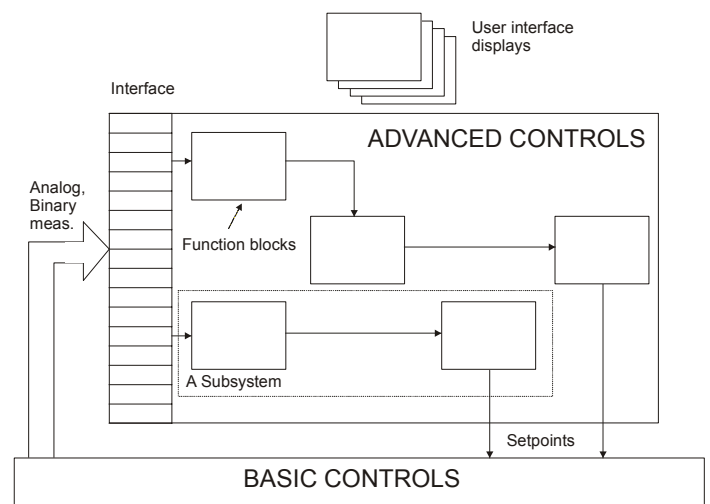


Fig.1 System diagram, which shows the application architecture

1. Problems in FBB technology

In the combustion of solid fuels, 90 % of disturbances arise from the fuel. Fuel quality, inconstant flow or asymmetrical feed cause variations. Normally the boiler itself and the air system function as they are designed, but proper handling of varying solid fuels is still an enigma. As the solid fuel burns quickly in the bed, and neither the amount nor quality of fuel are constant, there are always oscillations in the combustion. Rapid load changes and imbalance in fuel distribution magnify this effect. These combustion oscillations cause increased emission levels (Joronen 2000).

Emissions are produced as a result of complex chemical reactions. These reactions are a natural part of combustion and cannot be optimized independently of one another. The principle effects of some operating parameters cannot be easily decoupled from each other. Combustion management has to take in to consideration all these effects. Fluidized bed combustion, as any combustion process, is multi-variable and the cross effects between variables need to be taken in to account (Joronen 2000).

Parameter (horizontal axis)	Effect (Vertical axis)			
	1- η_c	SO ₂	N ₂ O	NO
Solids residence time (recirculation)	↘	↘	→	→
Calcium addition, Ca/S molar ratio	→	↘	→	↗
Bed temperature	↘	↘	↘	↗
Excess air	→	→	→	→
Air Staging	→	→	→	→
Pressure	→	→	→	→

Fig.2 The phenomenal effects of increases in operating parameters in CFB.

Naturally CO-emissions are low in FBB, so the oxygen level can be quite low. When O₂-level decreases, the probability of carbon monoxide concentration in the flue gas increases. If there is not enough air, combustion is incomplete and there will be unburned particles and carbon monoxide (CO) in the flue gas. But even if the total airflow is sufficient, uneven distribution may cause production of CO. For this reason it is important to assure of uniform mixing and turbulence in the whole furnace. Combustion can be incomplete also if the fuel feed increases too rapidly compared to maximum speed of change in airflow (Joronen 2000). Combustion speed of CO and unburned particles can be kept in the acceptable range while the bed temperature is kept high, even when burning low-calorimetric fuel.

Thermal nitrogen oxides (NO_x) reaction speed is highly dependent on the combustion temperature. To avoid NO_x generation, the temperature should be as low as possible and kept constant. Especially, there should not be any hot spots in the furnace as these produce nitrogen oxides. Nitrogen oxides can be reduced back to harmless nitrogen gas (N₂) in low-oxygen combustion conditions. In a BFB, air distribution can easily be staged so that these reductive conditions are reached. The staging has physical limits; the temperature and air ratio needs to be high enough for combustion in the upper furnace. In a CFB the N₂O-emission can be remarkable. The correlations between combustion parameters and NO_x- and N₂O-emissions are inverse (Åmand 1994, Leckner 1998).

In FBB, sulfur capture is easy to realize with limestone injection. Reaction speed and efficiency are highly dependent on the bed temperature. Variations in bed temperature decrease the efficiency of sulfur dioxide capture, increasing SO₂-emissions and consumption of limestone. The reaction uses oxygen, so conditions need to be oxidative. In reductive conditions gypsum, the end product of the sulfur reaction, releases already captured sulfur dioxide. If the oxygen concentration overall or locally decreases, sulfur emission increases. Therefore steady oxidative conditions are vital questions in SO₂-control. These conditions need to be taken care of even when load or fuel qualities are transient (Markkula et al 2000).

2. Solutions

The first task in an application delivery project is a careful process study. The study is required because of the different natures and states of plants. As a result of the study, solutions for the problems are defined. Good fuel and air controls are vital for optimal boiler operation. Any improvement in basic controls results directly in better combustion. The boiler is stabilized and running models are then implemented with coordinating controls. Combustion symmetry, combustion efficiency, CO-level, NO_x and SO₂-emissions are controlled and optimized with fuzzy controllers.

Fuel Power and Fuel Caloric Value Compensation

In plants using various fuels the caloric value may vary a lot, and compensation for fuel quality is needed. In the application the boiler load and air controls are changed on a fuel power basis. Fuel power (MW) of the solid fuel is continuously calculated according to the boiler balance. The caloric value is the fuel power divided by fuel flow. The calculated caloric value is a good estimate of the fuel quality.

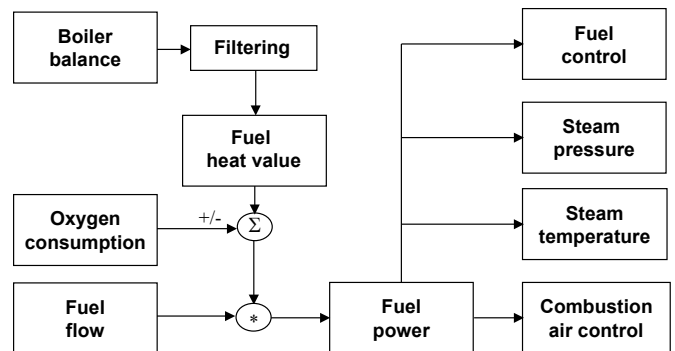


Fig.3 Picture of total fuel power calculation and main controls

Total Air Calculation and Air Distribution Model

Calculation of total combustion air is based on fuel power. This means that the changes in fuel flow caused by a change in caloric value is compensated mathematically. The air/fuel power-ratio is always steadier than air/fuel flow-ratio. Running models for air distribution; the recipes are implemented. The filtered airflow is divided to air registers by recipes. Recipes are tuned for different fuel mixes and operating situations. The use of basic recipe unifies the operation and makes optimization possible. Total combustion air fuzzy control guarantees that the amount of combustion air is always correct, so that the O₂-controller may operate with full control range.

Symmetry

Symmetry means homogeneous combustion in the furnace. Imbalance can be inferred from oxygen levels, flue gas and steam temperatures. Symmetry fuzzy control balances the fuel feed.

O₂/CO-Optimization

In FBB the oxygen concentration in the flue gas is controlled by secondary airflow. Basic set points for airflows are derived from the model and they vary by boiler load level. O₂/CO- fuzzy optimization corrects the oxygen level so that the loss due to excess air and carbon monoxide is minimized. The idea is to minimize the combustion air amount as near to the limit of complete and incomplete combustion as possible, considering the emission limits. The efficiency increases and needed fan power decreases. The change in excess air has effects also on furnace temperature, nitrogen emissions, sulfur capture, but the effects are handled with limitations to O₂-level.

Bed and Furnace Temperature Controls

Bed temperature fuzzy control is used to keep the temperatures in the bed and in the freeboard within acceptable limits. The fuzzy controller controls ratios between flows of air and recirculated flue gas (if used). The control of temperatures in the bed and in the freeboard is important for efficient burning and sulfur capture with limestone. Safety limitation of the high temperatures in the bed (and cyclone) may also be needed.

NO_x-Control

The NO_x fuzzy control is based on O₂-level and airflow staging. The control functions together with the O₂/CO-optimization and the bed temperature control. In some cases NO_x emission is controlled primarily with ammonia (SNR), then the aim is to save ammonia with air distribution and O₂-level.

SO₂-Control

The SO₂ fuzzy control is based on control of limestone. The reaction conditions are the cross effects taken in to account in other fuzzy controls, so that the use of limestone is minimized. Reaction kinetic and efficiency depend on bed temperature and chemical composition. The fuzzy bed temperature controls the bed temperature; bed chemistry is affected by NO_x-control.

3. The Structure of Fuzzy Control

The structure of fuzzy controllers used is similar and as simple as possible. Each controller inputs 1 - 5 measurements and has one control output [MISO]. These fuzzy controllers can be divided into three sub-functions: fuzzification, rule base and defuzzification.

In fuzzification the values of selected measurement are classified to fuzzy sets. In practice this means a calculation of membership values to fuzzy sets. The fuzzy sets are named illustratively, such as low, normal and high. To make the fuzzy control easy to understand, 3 - 5 triangular membership functions are used, even though the theory does not bound the number or shape of membership functions.

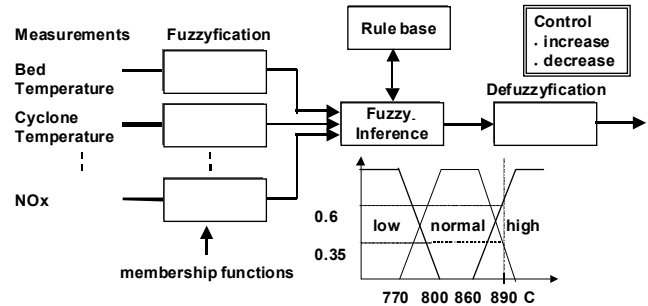


Fig.3 principle picture of the fuzzy controlled structure used in application

The rule-base consists of several if-then rules, which have been defined through expertise or a fuzzy model. In the application the reasoning is made by min-operator; the rule's truth-value is the smallest of the conditions effecting the rule. Rules have independent weighting value, which can be understood also as fixed truth-value weighting. The weighting values are thought as increments of control objects scaled between -1 to 1. The sign tells if the object of the control should be either increased or decreased.

In defuzzification the output is proportional to the sum of the absolute value of the weights. The final increment x_p is simply calculated through all rules 1 to n ,

$$x_p = \frac{\sum_{i=1}^n x_i \mu_i}{\sum_{i=1}^n |x_i|} \quad (1)$$

in which x_i are the weighting values and μ_i are the truth-values of the rules.

Because of the chosen defuzzification method and construction of the fuzzy reasoning the rule base can be incomplete. It is noteworthy that the rules, which are not needed, have 0 weight. So two rules, one for a positive increment and the other for a negative increment realize a functional rule base. This presumes that the rules are constructed so that the only exceptional situations that need control are addressed. If none of the rules is fired the situation is considered to be OK. The coordinate controls take care of the systematic relations.

4. Results

The advanced controls of FBB have provided good results. The applications are in continuous use, the boilers are easier to operate and emissions have decreased dramatically. The benefits achieved by better management of combustion are multi-faceted. The deviations and levels decrease, and also the process is operated more smoothly. In some cases steam production capacity can be increased. One clear result is that the operation styles between shifts are standardized.

The first advanced control application was implemented to the world's north-most CFB boiler in Rovaniemen Energia's Suosiola power plant in 1997. The boiler is peat and park fired and produces electricity and district heat. StoraEnso's Imatra mills BFB fuzzy combustion management has been used since 1997. The boiler was at the time of commissioning the world's biggest FBB, the production capacity is 72 kg/s, 84 bar steam. The boiler utilizes the mill's bark, paper waste and sludge. The third application was made to StoraEnso's Anjala papermill's boiler, which was modernized, from a grate boiler to a FBB in 1995. This boiler utilizes

mill's own bark, sludge and some RDF (Refuse-Derived Fuel).

In the Rovaniemi CFB emission levels were not any problem, the main focus was in safety limitations of the furnace temperatures and in increasing the automation level. In Rovaniemi CFB the oxygen level has decreased by 0.5 % and the NO_x -level because of this. The bed and cyclone temperatures are under control despite the load level or fuel calorific value and the combustion is automatically controlled. In BFB's Imatra and Anjala decreasing CO and NO_x emissions were the main task. They came up because of varying fuel and fast load changes. The automation level naturally increased. In BFBs the amount of time that CO exceeds emission limits has decreased by approximately 70 % per annum, and the standard deviation has decreased to one third. NO_x -emission has dropped by 18 - 25 %. At the same time efficiency has increased by means of decreased O₂ concentration in the flue gas and stabilized bed temperature, which ensures lower UBC [unburned coal]. In BFBs the combustion is automatically controlled.

At Imatra BFB due to using the advanced control concept, the time when CO exceeded the emission limit (CO over 250-ppm % of time) has in the long run decreased 67 % and the standard deviation has dropped 70 %. Just after the delivery of the control application the drop was about 77 %, but after a while the level tends to rise. The nitrogen oxides (NO_x) emission has come down 18 % and standard deviation of NO_x-emission limit exceeding has dropped to one fourth. Just after delivery the drop was about 29 %. O₂-level has decreased 5 % and its standard deviation 20 % and CO-emissions have been in good control

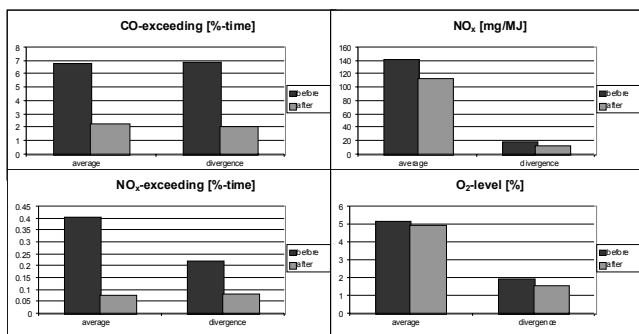


Fig.5 Results from StoraEnso Imatra mill's BFB

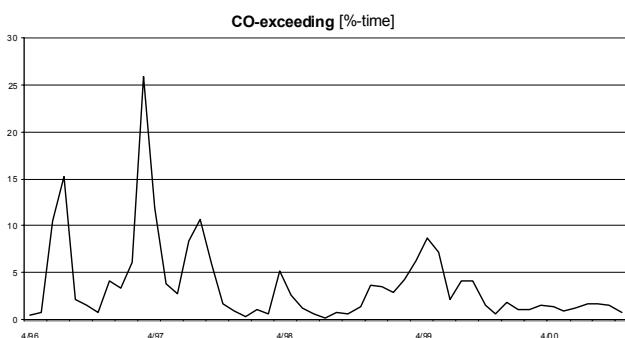


Fig.6 Trend of the portion of the time CO exceeding the emission limit

E.ON, UK Ltd. Kemsley could reach impressive results by the use of upper level fuzzy controls. There a fluidized bed boiler has to burn sludge and plastic waste. Fuzzy logic could increase the waste incineration by 15% with equivalent reduction in gas consumption. That means on one hand more income and on the other hand additional savings. (Crowhurst 2005)

Fortum Säteri Power Plant in Finland can report a similar success story. There the fluidized bed boiler has to burn peat, coal, sawdust, sludge, industrial waste, animal bones

and gas. (As supporting fuel) This mix is already a very challenging task for the upper level control, because of high variations in the fuel heating values. Nevertheless the result can be highlighted. Fuzzy logic could decrease the supporting gas consumption by 25%. In parallel the throughput of waste was increased. The payback time for the fuzzy control was about a month. (Jalkanen 2005)

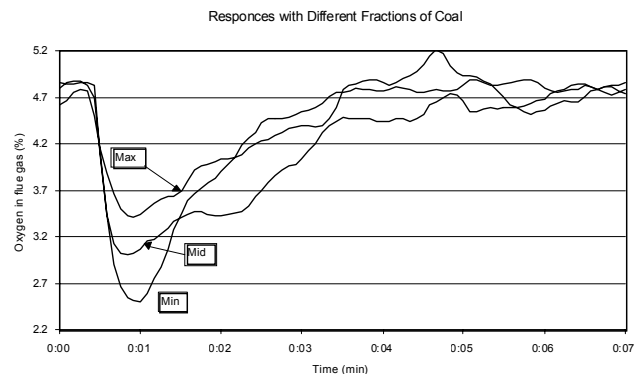


Fig.7 Three impulse responses with different fractions of fuel in a CFB

Conclusions

The increase of automation level can offer valuable financial and environmental impacts in industrial and utility boilers. A disturbance-free boiler is more reliable and more economical to use. Combustion is more stable and environmental emissions are radically reduced. We foresee tight process control having even greater value as the processes grow more complex and the environmental demands continue to tighten up. Basic research is utilized to create new more sophisticated applications to match future demands.

References

- [1] ÅMAND, L.-E. (1994): Nitrous Oxide Emission from Circulating Fluidized Bed Combustion. Dr. Thesis, Chalmers University of Technology, Göteborg, Sweden.
- [2] CRISWELL R. L. (1980): Control Strategies for Fluidized Bed Combustion. InTech, January, pp. 37 - 43.
- [3] CROWHURST R. (2005): Kemsley Reference Quote, E.ON UK., Kemsley Mill, England.
- [4] HUPA M. and MATINLINNA J. (1998): LIEKKI 2 Combustion and Gasification Research Program. Technical Review 1993 - 1998, vol.1. Rep. L98-3. Turku, Finland (Internet: <http://noon.abo.fi/Ook/Pages/Liekki.shtml>).
- [5] HUPA M. (2000): Studying the chemistry of combustion processes. Energy in Finland, Helsinki.
- [6] JORONEN, T. (2000): Päästöjen vähentäminen automaation avulla (Reducing emission by means of automation (in Finnish)), Energia kongressi, Tampere, Finland.
- [7] JALKANEN J. (2005): Fortum's Säteri Power Plant, Metso Automation Customer Magazine Volume 1 2005, Finland.
- [8] KARPPANEN E. (2000): Advanced control of an industrial circulating fluidized bed boiler using fuzzy logic. Department of Process and Environmental Engineering, University of Oulu, Finland.
- [9] KEYES, M. A. and KAYA, A. (1984): Applications of Systems Engineering to Control Fluidized-Bed Boilers. Flu-

idized bed combustion and applied technology; The 1st int. symp., Ed. Schwieger, R. G., pp. III- 147-171.

[10] KOKKO, A. and NIEMELÄ, J. (2000): World's largest biofuel fired CFB boiler for Alholmen's Kraft. Power-Gen 2000 Europe Conference Proceedings, Helsinki, Finland.

[11] KORTELA, U., IKONEN, E., KOTAJÄRVI, H. and HEIKKINEN, P. (1994): Modeling, Simulation and Control of Fluidized Bed Combustion Process. International Journal of Power and Energy Systems, Vol. 14, No. 3.

[12] LECKNER, B. (1998): Fluidized Bed Combustion: Mixing and Pollutant Limitation. Department of Energy Conversion, Chalmers University of Technology. PII: S0360-1285(97)00021-C, Göteborg, Sweden.

[13] MARKKULA, E., PYYKKO, J., JORONEN, T. and NEUBERT, R. (2000): Optimierung und Regelung der Verbrennung in Müllverbrennungsanlagen mit Hilfe von Fuzzy-Regelungen," (The Optimization and Control in Fluidized Bed Boilers with help of Fuzzy control), VGB-Konferenz "Thermische Abfallverwertung 2000", Essen, Germany.

[14] NYSTRÖM, P. (1983): Leijukerros poltto ("Fluidized Bed Combustion" (in Finnish)). Säätötekniikan prosessiovellukset Seminaariesitelmät 1983, Ed. Kortela, U. and Joensuu, J., Rep. 50, Helsinki University of Technology, Control Engineering Laboratory.

[15] PYYKKÖ, J. and UDDFOLK, J. (1997): Leijukattilan palamisen hallinta sumean logiikan avulla (Combustion management of FBB with fuzzy control (in Finnish)), Automaatiopäivät, Helsinki, Finland.

[16] RAATIKAINEN, T. (2000): Influence of Equipment Operation and Performance Deterioration on Power Plant Economy. Lappeenranta University of Technology, Department of Energy Technology.

[17] TUOVINEN, M. and KORTELA, U. (1988): Development of New Control Strategies for Reduction of Nitrogen

and Sulphur Oxide Emission in Fluidized Bed Combustion," Energy Options for the year 2000, Contemporary Concepts in Technology and Policy, Delaware, USA.

[18] U.S. Department of Energy (2000): Advanced Electric Power Generation Fluidized-Bed Combustion; JEA Large-Scales CFB Combustion Demonstration Project, Clean Coal Technology, Program Update.

Dr.Tech. Tero Joronen

Principal Scientist
Metso Automation Oy
Energy and Process Systems
Lentokentäkatu 11
33101 Tampere, Finland
Tel.: +358 20 483 8807
Fax: +358 20 483 8943
E-mail tero.joronen@metso.com

Dipl. Ing. Rupert Kerschbaum

Areas Sales Manager
Metso Automation Ges.m.b.H
Energy and Process Systems
Franzosengraben 12
1030 Vienna, Austria
Tel.: +43 1 79552-355
Fax: +43 1 79552-9355
E-mail rupert.kerschbaum@metso.com